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**METHOD FOR PRODUCING A PALLADIUM-
CONTAINING HYDROGENATION CATALYST**

Technical field

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The invention relates to physical chemistry and can be used for adjusting the rate of autocatalytic hydrogenation reactions.

Background art

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The hydrogenation reactions relate to basic industrial processes that are usually realized over a catalyst, in particular, for the synthesis of alicyclic and cyclic saturated organic compounds, high-quality benzene, etc.

20 According to the written publications known in the art (see Grove D.E. Plat. Met., 2002, 46, (2) 92), about 75% of the industrial hydrogenation processes are realized over the Pd/C catalyst, which contains 5% of metal palladium. The rich variety of palladium's catalytic properties allows using it in almost all reactions necessary for
25 the organic synthesis. Therefore, at present, Pd/C is the most suitable system for realizing the processes of the catalytic organic synthesis.

A known method for producing a palladium-containing hydrogenation catalyst consists in reducing divalent palladium from the initial compound thereof and precipitating the thus reduced palladium on a carbon material, wherein the initial compounds are embodied in the form of Pd (II) complexes, see Tsuji J. Palladium reagents and catalysts-innovations in organic syntheses. John Wiley & sons, Chichester. 1995. 595p.; Grove D.E. Plat. Met., 2002, 46, (1) 48.

Another known method for producing a palladium-containing hydrogenation catalyst consists in reducing divalent palladium from the initial compound thereof and precipitating the thus reduced palladium on a carbon material, wherein the initial compound is embodied in the form of palladium chloride (II), see H.M.Colquhoun, Y.Holton, et alii, "New Pathways for Organic Synthesis" («Новые пути органического синтеза»), translated from English by M.S. Ermolenko and V.G. Kiseleva, Moscow, «Химия» ("Chemistry"), 1989, 361 p., 2nd paragraph counting from the top of the page.

The palladium chloride (8.2 g) solution in hydrochloric acid (20 ml of concentrated acid in 50 ml of water) is heated during 2 hours, then added, while constantly stirring, to a hot (80⁰C) coal suspension in water (93 g of coal in 1.2 l of water), wherein the coal has previously been washed with nitric acid.

Coal of almost any type can be used, provided that said coal has a sufficiently large specific surface area, has been washed with nitric acid (10%) during 2-3 hours, subsequently washed with water in order to eliminate the acid, and dried at 100⁰C. Then the formaldehyde is added (8 ml of 37% solution) and subsequently the sodium hydroxide solution

is added until a strong alkaline reaction is achieved. After 10 minutes the thus obtained catalyst is filtered out, washed with water (10x250 ml) and vacuum dried over calcium chloride. The palladium outlet equals 5% for 93-98% coal.

5 This method is taken as a prototype of the present invention.

 The disadvantage of said method is in that the catalyst produced according to this method exhibits a low catalytic activity and operates only at high temperatures (higher than 60⁰C) and high pressure (higher than 5 gauge atmospheres). The reason for said disadvantage is the
10 difficulty of activation of the reaction centers of the catalyst produced according to the prototype method.

Summary of the invention

15 It is an object of this invention to develop a method for producing a palladium-containing hydrogenation catalyst, which exhibits a higher catalytic activity and operated in softer conditions (at a room temperature and a normal (atmospheric) pressure).

 According to the present invention there is provided a method for
20 producing a palladium-containing hydrogenation catalyst, which consists in reducing divalent palladium from the initial compound thereof and precipitating the thus reduced palladium on a carbon material, wherein the initial compound is embodied in the form of tetra aqua-palladium (II) perchlorate. The reduced palladium is precipitated
25 on a nano-carbon material which can be embodied in the form of fullerene C₆₀, carbon nanotubes, cathodic deposit and the mixture of C₆₀

and C₇₀ fullerenes at the following ratio thereof: 60-80 mass % fullerene C₆₀ and 20-40 mass % fluorine C₇₀.

The applicant hasn't found any sources of information containing data on engineering solutions identical to the present invention. In
5 applicant's opinion, that enables to conclude that the invention conforms to the criterion "novelty" (N).

The distinguishing characteristics of the present invention enable to achieve an important engineering result, which consists in that the embodiment of the initial compound in the form of tetra aqua-palladium
10 (II) perchlorate allows producing reduced palladium with high dispersion ability, and the precipitation of the reduced palladium on a nano-carbon material allows keeping the palladium in nano-clustered form.

Said conditions significantly increase the catalytic activity of the
15 substance produced by the realization of said method and make it possible to conduct the catalysis process at a room temperature and normal atmospheric pressure.

The applicant hasn't found any sources of information containing data on the influence of said distinguishing characteristics on the
20 engineering result achieved through the application thereof. In applicant's opinion, that enables to conclude that the invention conforms to the criterion "inventive step" (IS).

Brief description of the drawings

The present invention is illustrated, by way of example, with reference to the accompanying drawings in which:

Figure 1 is a scheme of the plant for the realization of the inventive method for producing a palladium-containing hydrogenation
5 catalyst;

Figure 2 is a time graph of the volume of the absorbed gas mixture for various hydrogenation reactions over a catalyst produced by means of the method according to claim 2:

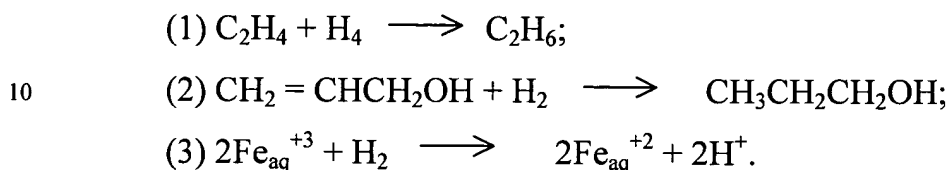


Figure 3 is identical to figure 2, but the catalyst is produced by means of the method according to claim 3;

Figure 4 is identical to figure 2, but the catalyst is produced by
15 means of the method according to claim 4;

Figure 5 is identical to figure 2, but the catalyst is produced by means of the method according to claim 5.

Preferred embodiment

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The plant for realization of the inventive method comprises a reactor 1 provided with a mixer 2. Hydrogen is contained in the cylinder 3. The reactor 1 is connected to the manometric plant 4.

In the first specific embodiment the method is realized in the
25 following way.

2.0 liters of distilled water are placed in the reactor 1. Then 600 mg of nano-carbon material are introduced, in particular, fullerene C₆₀. Then 5.22 ml of $5.7 \cdot 10^{-2}$ m [Pd(H₂O)₄(ClO₄)₂] solution are added, said solution containing 0.7 m of chloric acid, and the mixture is stirred
 5 during 0.5 hour. Then the divalent palladium is reduced by passing it through the prepared hydrogen solution during 2 hours.

The sediment is filtered out by means of the Shott filter, repeatedly washed with distilled water and dried in a vacuum desiccator over P₂O₅ during 2 days (48 hours). The catalyst outlet equalled 98 –
 10 99% (catalyst I).

The second specific embodiment (catalyst II) differs from the first one only in that the nano-carbon material is embodied in the form of carbon nanotubes; in the third specific embodiment (catalyst III) the nano-carbon material is embodied in the form of cathodic deposit; in the
 15 fourth specific embodiment (catalyst IV) the nano-carbon material is embodied in the form of the mixture of C₆₀ and C₇₀ fullerenes at the following ratio thereof:

fullerene C₆₀ - 60 – 80 mass %

fullerene C₇₀ - 20 – 40 mass %

20 Each catalyst produced was tested in all three hydrogenation reactions mentioned above. For this, 10 mg of catalyst were placed in the solution and then corresponding substance was added: 10 ml of distilled water for reaction (1), 10 ml of 0.01 aqueous solution of ferric sulphate for reaction (2), 10 ml of 0.002 aqueous solution of allyl
 25 alcohol for reaction (3). For reaction (1), the reactor was filled with the mixture of ethylene and hydrogen at the volume ratio of 1 : 1; for

reactions (2) and (3), the reactor was filled with hydrogen. The reactions were conducted at a temperature of 18 – 25⁰C and a normal atmospheric pressure. The rates of the reaction (1), (2) and (3) were measured by the time variation of the absorbed gases' volume over the catalysts I, II, III, 5 IV (see figure 2, 3, 4, 5 respectively).

For comparison purposes, the rates of the hydrogenation reactions, conducted in similar conditions, but over industrial catalyst Pd/C, were measured. In reaction (1) the rate did not exceed 10 – 12% of the hydrogenation rate over catalysts I, II, III, IV, in reaction (2) 10 almost no hydrogenation was observed, in reaction (3) no difference in the hydrogenation rate was observed.

Industrial applicability

15 Known simple industrial equipment and materials common in the art are used for the realization of the method, which enables to conclude that the invention conforms to the criterion “industrial applicability” (IA).